

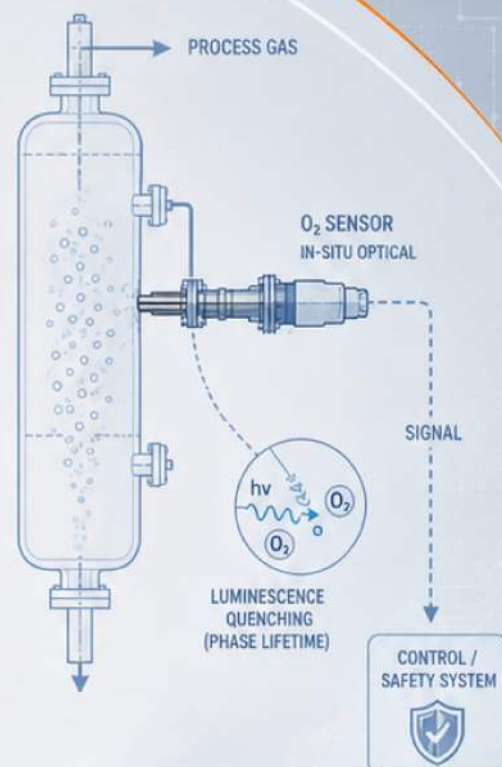
THE ENGINEERING GUIDE TO OXYGEN MEASUREMENT

Second revised engineering handbook edition

Gas-phase and dissolved oxygen measurement
from trace ppm to 100% O₂

*Applications in hydrogen, natural gas, biogas, refineries,
petrochemicals, industrial gases, combustion and fuel cells*

Modcon Systems Ltd. | Engineering Handbook Edition | Rev.2.0 | June 2026



TRACE PPM
TO 100% O₂



IN-SITU &
EXTRACTIVE



FAST
RESPONSE



SAFETY
INTEGRITY



REDUCED
MAINTENANCE

OXYGEN PERFORMANCE OVERVIEW

O₂ CONCENTRATION
20.90%

RESPONSE TIME (T90)
2.8 s

STABILITY (24H)
±0.05%

SIGNAL QUALITY
98.7%

SENSOR TEMPERATURE
48.6 °C

CALIBRATION STATUS
OK

OPTICAL QUENCHING PRINCIPLE



MEASUREMENT LOOP



APPLICATIONS ACROSS INDUSTRIES



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1. Executive engineering summary

Oxygen measurement is often treated as an instrument purchase. In demanding process service it is closer to a small safety project. The analyzer, tapping point, sample path or insertion arrangement, pressure control, diagnostics, calibration practice and trip logic all decide whether the number on the screen is useful or merely decorative.

The right technology depends on the duty. A combustion stack, a hydrogen electrolyzer, a natural gas pipeline and a bioreactor may all ask for oxygen, but they do not ask for the same measurement. The required answer may be ppmv, volume percent, oxygen partial pressure, dissolved oxygen, rate of change or a diagnostic proof that the measurement has not quietly become blind.



Good oxygen measurement is a complete loop, not only a sensor selection exercise.

Bias, delay, diagnostics and proof testing must be assessed from process tapping point to final protective action.

Question	Why it matters	Typical engineering consequence
Is oxygen a quality variable, a control variable or a safety variable?	The acceptable response time, diagnostics and proof testing differ strongly.	SIF/SIS duties require a safety requirement specification and validated safe-state behaviour.
Is the sample clean, wet, sour, dusty, hot or high pressure?	Many oxygen technologies are excellent only inside their correct operating envelope.	Matrix control and mechanical installation may matter more than analyzer nameplate accuracy.
Is the measurement at trace ppm or percent level?	Air ingress and adsorption/desorption can dominate trace readings.	Dead volume, leaks and tubing materials become part of the measurement error budget.
Can the measurement be made directly in the process?	In-situ measurement can remove sample delay and reduce leak paths.	Representative location and fouling control become the main design tasks.
What happens when the analyzer fails high or fails low?	The dangerous failure direction is application-specific.	Trip architecture, diagnostics and proof tests should be designed around the real hazard.

2. Oxygen measurement fundamentals

2.1 Units and what they really mean

Oxygen may be reported as volume fraction (% v/v or ppmv), mole fraction, partial pressure, mg/L for liquids, ppb for very low dissolved oxygen, or as oxygen saturation. These units are not interchangeable unless pressure, temperature, water vapour and matrix conditions are known.

Term	Meaning	Engineering comment
% v/v	Volume percent in a gas mixture. For ideal gases it is normally equivalent to mole percent.	Common for air, combustion, inerting and high oxygen streams.
ppmv	Parts per million by volume. 1 ppmv = 0.0001% v/v.	Useful for trace oxygen in hydrogen, nitrogen, natural gas and specialty gases.
Partial pressure	The pressure contribution of oxygen in a mixture.	Oxygen chemical activity and many sensor responses are related to partial pressure, not only concentration.
mg/L	Mass of dissolved oxygen per litre of liquid.	Depends strongly on temperature, salinity, pressure and liquid composition.
% saturation	Dissolved oxygen relative to equilibrium with a reference atmosphere.	Convenient for water and biological processes, but less useful for high-pressure process liquids.
T90	Time for the indicated value to reach 90% of a step change.	Must include process transport and sampling delay, not only sensor cell response.

2.2 Pressure, temperature and water vapour

A dry gas reading and a wet gas reading can differ even when the dry-gas oxygen content has not changed. Water vapour dilutes dry gas components. Similarly, pressure changes alter oxygen partial pressure and may change sensor response unless compensation is built into the measurement model.

An example applicable to partial pressure-based measurements: A gas mixture containing 1% O₂ has an oxygen partial pressure of approximately 0.01 bar at atmospheric pressure, but already 1 bar when the total pressure is 100 bar. Although the oxygen concentration remains unchanged, the oxygen partial pressure – and therefore the sensing conditions for the measurement technology – changes by a factor of 100.



Practical implication: For high-pressure hydrogen or natural gas, a measurement that is accurate at atmospheric pressure in the workshop may not be accurate in the pipeline unless the analyzer, calibration method and compensation model have been designed for pressure service.

2.3 Trace oxygen is mostly a sample system problem

At ppm levels the analyzer is rarely the only error source. Air ingress through fittings, permeation through tubing, adsorption and desorption on wetted surfaces, stagnant pockets, regulator volume, filter housings and poorly purged calibration lines can all create oxygen readings that are real in the sample system but not representative of the process.

- Keep wetted volume low and avoid unnecessary filters, regulators and long tubing runs.
- Use materials and seals compatible with the gas, pressure, contaminants and area classification.
- Validate leak tightness using a method sensitive enough for the required ppm level.
- Purge calibration and sample lines long enough to clear dead legs and adsorbed oxygen.
- Record as-found and as-left data; a calibration that starts by adjusting everything hides useful evidence.

Oxygen may be specified as volume fraction (ppmv or % v/v), partial pressure, or dissolved concentration (mg/L or ppb). In gases, pressure and temperature influence density and partial pressure relationships; in liquids, dissolved oxygen depends on solubility, mass transfer, and temperature. Trace oxygen applications are frequently limited by air ingress and adsorption/desorption in the sample path.

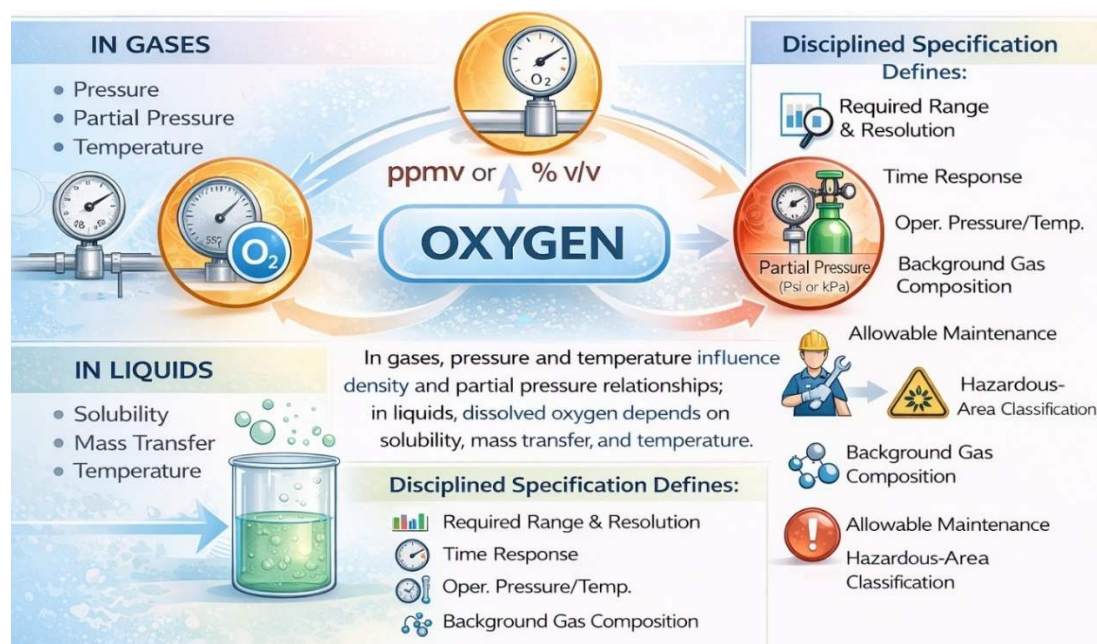


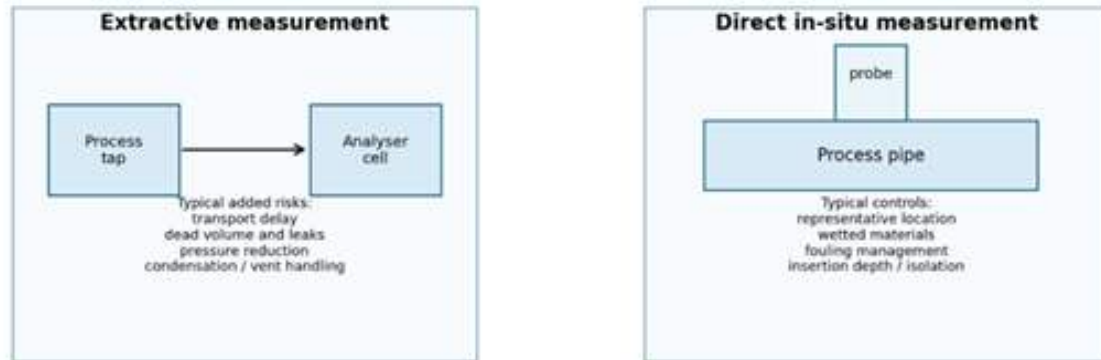
Fig. 1 – Oxygen Measurement Fundamentals

A disciplined specification defines: required range and resolution; time response; operating pressure/temperature; background gas composition; allowable maintenance; hazardous-area classification; and the consequence of undetected failure.

Term	Meaning	Engineering comment
% v/v	Volume percent in a gas mixture. For ideal gases it is normally equivalent to mole percent.	Common for air, combustion, inerting and high oxygen streams.
ppmv	Parts per million by volume. 1 ppmv = 0.0001% v/v.	Useful for trace oxygen in hydrogen, nitrogen, natural gas and specialty gases.
Partial pressure	The pressure contribution of oxygen in a mixture.	Oxygen chemical activity and many sensor responses are related to partial pressure, not only concentration.
mg/L	Mass of dissolved oxygen per litre of liquid.	Depends strongly on temperature, salinity, pressure and liquid composition.
% saturation	Dissolved oxygen relative to equilibrium with a reference atmosphere.	Convenient for water and biological processes, but less useful for high-pressure process liquids.
T90	Time for the indicated value to reach 90% of a step change.	Must include process transport and sampling delay, not only sensor cell response.

3. System view: analyzer, sampling and installation

The complete oxygen measurement loop starts at the point where the process contacts the measurement system. A sample that is diluted, delayed, condensed, contaminated or thermally altered cannot be rescued by a clever transmitter.



3.1 Extractive systems

Extractive oxygen systems remain appropriate where the process is too hot, dirty, inaccessible or mechanically unsuitable for direct measurement. They allow conditioning, filtration, pressure control and analyzer-house installation. The price is added delay, added failure modes and a higher maintenance burden.

Extractive design item	Good practice	Common failure mode
Sample tap	Use a representative location with velocity and mixing understood.	Stratified or stagnant sample gives plausible but wrong readings.
Pressure reduction	Control Joule-Thomson cooling, condensation and vent safety.	Condensation or regulator memory shifts trace oxygen.
Tubing	Minimise length and dead volume; use suitable materials.	Permeation or leaks dominate ppm measurements.
Flow control	Specify normal, minimum and alarmed flow.	Low flow gives slow response and poor purging.
Calibration gas	Use traceable gases close to operating range and matrix when possible.	Calibration gas uncertainty is larger than the process tolerance.
Vent and purge	Route safely according to gas hazard and area classification.	Hydrogen or toxic gas venting becomes a safety issue.

3.2 In-situ systems

In-situ measurement removes the sample transport path and can sharply improve time-to-detection. It is especially attractive where pressure reduction, hydrogen venting or sample conditioning creates more risk than value. It does not remove engineering discipline. It moves the main design effort to nozzle design, insertion depth, isolation, materials, fouling, diagnostic access and validation method.

In-situ design item	Engineering check
Location	Avoid dead legs, two-phase regions, poorly mixed headers and places where maintenance access creates a new hazard.
Mechanical interface	Define pressure rating, process connection, insertion length, isolation, removal method and material compatibility.
Fouling and condensation	Assess wax, liquid carryover, aerosols, salts, particulates and biological film; design inspection and cleaning access.
Electrical safety	Confirm hazardous area classification, equipment protection concept, cable glands, earthing and segregation.
Validation	Define how zero/span or bump tests will be applied without creating an unrepresentative test condition.

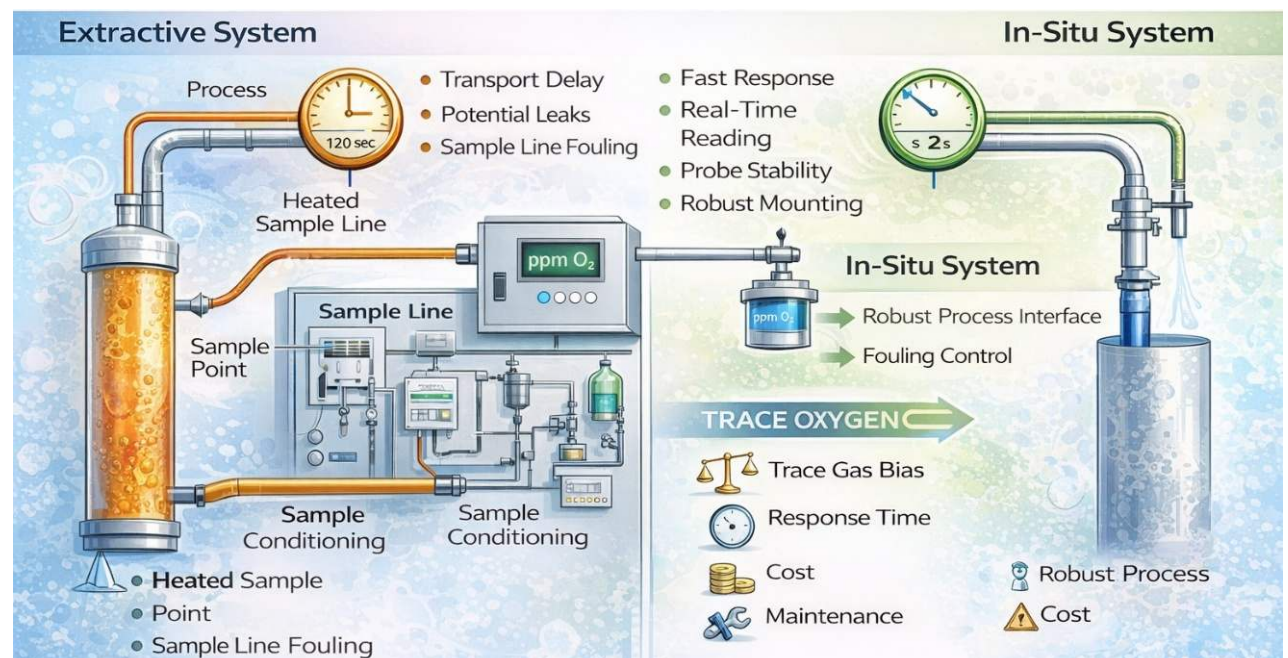


Fig. 2 – Extractive sampling system vs In-situ System

Oxygen analyzers must be evaluated as complete systems. Extractive systems add transport delay and introduce leak points; in-situ systems reduce delay but require robust process interfaces and fouling control. For trace oxygen, sample system design often dominates both bias and response time.

Key engineering controls include minimizing dead volume, verifying leak integrity, ensuring safe venting/purging, providing stable pressure/flow, and implementing diagnostics that indicate representativeness of the sample.

4. Gas-phase oxygen technologies

4.1 Electrochemical oxygen sensors

Electrochemical sensors use oxygen reduction at a cathode. In galvanic cells the reaction generates the signal; in polarographic cells an applied potential controls the reaction. Oxygen reaches the electrode by diffusion through a membrane or capillary barrier, so pressure, temperature, membrane condition and flow can affect response.

Strengths	Limitations	Best fit
Low cost, compact, sensitive at low ppm in clean gases, simple electronics.	Consumable chemistry, drift, poisoning risk, humidity and pressure sensitivity, limited diagnostics.	Portable verification, clean utility gases, non-SIF monitoring where routine replacement is acceptable.

Electrochemical oxygen sensors measure oxygen through reduction reactions at a cathode. Oxygen reaches the electrode by diffusion through a membrane or capillary barrier, making the signal fundamentally diffusion-limited.

Galvanic sensors are self-powered cells where oxygen participates in the electrochemistry. Polarographic sensors use an external bias voltage to control the cathode reaction. Both require stable membrane condition and compensation for temperature and pressure.

These sensors can be sensitive at low ppm levels in clean gases and are widely used in portable and low-cost fixed installations. The primary drawbacks are consumable life, drift, and susceptibility to poisoning from reactive gases and humidity.

In trace oxygen service, engineering success often depends more on leak integrity and sample design than on sensor resolution.

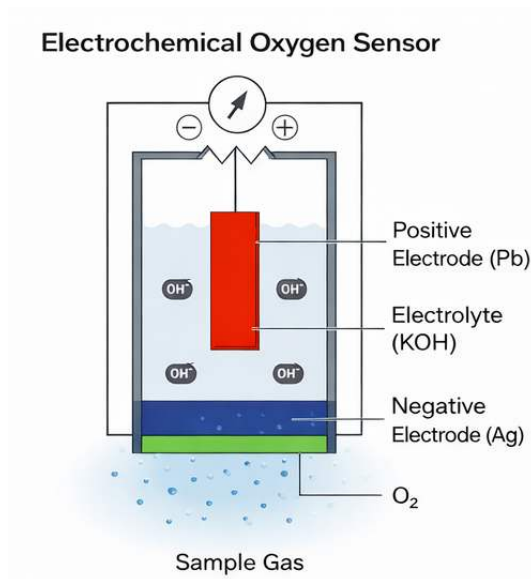


Fig. 3 – Electrochemical oxygen sensor (gas) – diffusion-limited cell

4.1.1 Safety integrity and SIL considerations

Electrochemical sensors generally provide limited intrinsic diagnostics for drift and poisoning. For safety-related use, apply redundancy (e.g., 1oo2), tight proof-test intervals, and conservative trip points. Treat the sample system as part of the SIF because air ingress and flow failures can dominate output.

4.1.2 Failure-mode-focused SWOT (with diagnostic coverage)

Dimension	Key points	Typical fail-high behavior	Typical fail-low behavior
Strengths	Low initial cost; compact; strong sensitivity in clean service; simple electronics; broad availability.		
Weaknesses	Consumable cell and electrolyte; drift/aging; sensitive to humidity, temperature, pressure/flow; poisoning risk.	Air ingress upstream; membrane damage increasing diffusion; calibration gas contamination.	Electrolyte depletion; cathode poisoning; membrane blockage; insufficient flow; flooding by moisture.
Opportunities	Portable verification; secondary measurements;		

	applications with frequent maintenance access.		
Threats	Undetected drift between checks; air ingress causes false high oxygen; poisoning causes false low; high lifecycle cost in harsh duty.	Air ingress upstream; membrane damage increasing diffusion; calibration gas contamination.	Electrolyte depletion; cathode poisoning; membrane blockage; insufficient flow; flooding by moisture.
Diagnostics / Proof testing	Typically limited. Improve diagnostic coverage with flow/pressure supervision, as-found/as-left trending, bump tests, and comparison to a diverse technology.		

4.2 Zirconia oxygen sensors

Zirconia sensors are high-temperature solid electrolyte devices. They compare oxygen activity at the process electrode with a reference side and produce a Nernst-type voltage. Their natural home is hot combustion and flue gas service, where fast percent-level oxygen feedback is needed.

Strengths	Limitations	Best fit
Fast in hot gases, mature combustion technology, strong signal for %O ₂ control.	Requires heater control, reference integrity, protection from thermal shock, reducing atmospheres and condensate.	Boilers, furnaces, fired heaters and emissions-related combustion optimisation.

Zirconia oxygen sensors operate as solid-electrolyte concentration cells at elevated temperature. With platinum electrodes and a reference gas, they generate a voltage governed by the logarithm of oxygen partial pressure ratio (Nernst behavior).

The technology is dominant in combustion and flue gas applications due to fast response at percent-level oxygen and compatibility with hot process environments.

Key sensitivities include thermal shock, soot/particulate deposition, condensation, and exposure to strongly reducing atmospheres. Heater control and reference-side integrity are central to stable measurement.

Applied within its intended domain with proper protection and diagnostics, zirconia provides robust control feedback for combustion efficiency and emissions strategies.

Zirconia (Nernst Cell) Oxygen Sensor

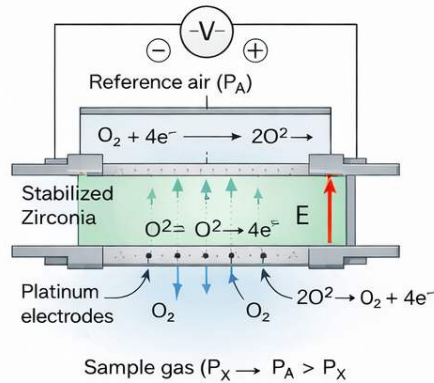


Fig. 4 – Zirconia (Solid Electrolyte / Nernst Cell) oxygen sensor

4.2.1 Safety integrity and SIL considerations

For safety-related combustion functions, integrate heater monitoring, temperature supervision, and plausibility checks. Consider redundancy when oxygen measurement prevents unsafe combustion conditions. Proof testing should validate reference integrity and response.

4.2.2 Failure-mode-focused SWOT (with diagnostic coverage)

Dimension	Key points	Typical fail-high behavior	Typical fail-low behavior
Strengths	Fast response in hot gases; mature technology; strong combustion compatibility; direct %O ₂ control variable.		
Weaknesses	Requires high-temperature operation; susceptible to condensation/thermal shock; electrode aging; protection required.	Reference path leak/contamination; temperature control error causing bias.	Heater failure; cracked electrolyte; condensation; electrode poisoning.
Opportunities	Boiler and furnace optimization; burner management support;		

	emissions monitoring contexts.		
Threats	Heater failure; reference contamination; fouling leading to sluggish response; misuse outside intended range.	Reference path leak/contamination; temperature control error causing bias.	Heater failure; cracked electrolyte; condensation; electrode poisoning.
Diagnostics / Proof testing	Moderate: heater current/temperature, impedance checks, EMF plausibility. Proof tests should include step response and reference-side checks.		

4.3 Paramagnetic oxygen analyzers

Oxygen is paramagnetic and is attracted into a magnetic field. Paramagnetic analyzers convert this property into a mechanical, pressure or thermal signal. They are selective to oxygen and non-consumable, but they normally require a clean, dry and well-conditioned sample.

Strengths	Limitations	Best fit
Selective to oxygen, stable in clean gas, fast response, no consumable cell.	Sensitive to vibration, pressure/flow changes, moisture, condensables and particulates depending on design.	Air separation, oxygen enrichment, inerting and clean dry process gases.

Paramagnetic analyzers use oxygen's attraction to magnetic fields. Implementations convert magnetic-force effects into a mechanical deflection or pressure signal proportional to oxygen concentration.

They are widely used for percent-level measurement in clean, dry gas streams such as oxygen enrichment, air separation, and inerting.

Practical performance depends strongly on stable sample conditioning: moisture, dust, condensables, and pressure/flow instability can introduce bias. In many plants, the sample system determines reliability.

For inerting, verify that the measurement location and sample transport reflect the hazardous condition within required time.

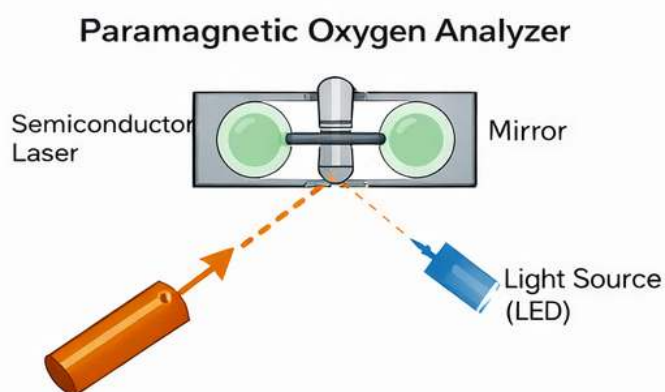


Fig. 5 – Paramagnetic oxygen analyzer – magnetic susceptibility principle

4.3.1 Safety integrity and SIL considerations

Paramagnetic analyzers can support safety functions in clean services when sample conditioning is robust and monitored. Intrinsic diagnostics can be limited; improve safety integrity with conditioning alarms, flow/pressure monitoring, and periodic gas checks.

4.3.2 Failure-mode-focused SWOT (with diagnostic coverage)

Dimension	Key points	Typical fail-high behavior	Typical fail-low behavior
Strengths	High selectivity to O ₂ ; non-consumable; stable in clean service; fast response.		
Weaknesses	Sensitive to pressure/flow and contamination; some designs sensitive to vibration/temperature gradients.	Pressure regulation instability; mechanical imbalance; temperature gradient bias.	Sample dilution; moisture ingress; blocked filters reducing flow; downstream leaks.
Opportunities	ASU and enrichment; clean-gas inerting; long-term monitoring where conditioning is reliable.		
Threats	Conditioning failures; dilution/leaks; installation-induced vibration and thermal gradients.	Pressure regulation instability; mechanical imbalance; temperature gradient bias.	Sample dilution; moisture ingress; blocked filters reducing flow; downstream leaks.
Diagnostics / Proof testing	Often modest. Improve DC with conditioning instrumentation (dew point, flow, pressure), plausibility checks, and scheduled proof tests.		

4.4 Tunable diode laser absorption spectroscopy

TDLAS measures absorption at an oxygen spectral feature. It can be configured in-situ or in an extractive cell. Its advantages are speed, no consumable sensing element and strong diagnostics from signal strength and spectral fit. Its weaknesses are optical access, window fouling, alignment and possible spectral interference.

Strengths	Limitations	Best fit
Very fast response, in-situ option, no consumables, strong diagnostics.	Needs optical path, alignment and window health; can be challenged by dust, droplets or beam steering.	Fast purge/inerting detection, combustion zones where optics can be protected, harsh service where extractive sampling is undesirable.

TDLAS measures oxygen by tuning a diode laser across an oxygen absorption feature and interpreting the attenuation using absorption physics. The method can be applied in-situ or in extractive cells.

TDLAS is valued for very fast response and the ability to reduce sample-system risks by measuring directly in the process. It avoids consumable sensing elements.

Engineering challenges include window fouling, optical alignment, beam steering, and signal-to-noise in dusty or wet environments. These are mitigated by mechanical design, purge strategies, and using optical health diagnostics as primary protection layers.

For fast transients such as purge and inerting upsets, in-situ TDLAS can materially improve time-to-detection when the optical path is representative.

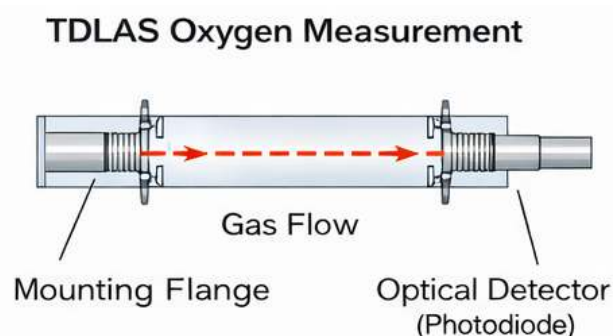


Fig. 6 – TDLAS oxygen measurement – laser absorption path

4.4.1 Safety integrity and SIL considerations

TDLAS can provide high diagnostic coverage via signal strength and spectral fit metrics. In SIL use, treat optical degradation and out-of-model conditions as safety-relevant alarms/trips and define proof tests that validate both measurement and diagnostics.

4.4.2 Failure-mode-focused SWOT (with diagnostic coverage)

Dimension	Key points	Typical fail-high behavior	Typical fail-low behavior
Strengths	Very fast response; no consumables; in-situ capability; strong selectivity; rich diagnostics.		
Weaknesses	Requires optical access and alignment; window condition critical; higher engineering effort.	Baseline fitting error; detector saturation; stray light artifacts.	Window fouling; beam blockage; reduced signal; path length change unnoticed.
Opportunities	Fast safety detection; harsh monitoring where extractive sampling is risky; modernization of inerting systems.		
Threats	Fouling/condensation blocking optics; misalignment after maintenance; ignoring diagnostics.	Baseline fitting error; detector saturation; stray light artifacts.	Window fouling; beam blockage; reduced signal; path length change unnoticed.
Diagnostics / Proof testing	Typically high. Proof tests should validate diagnostic thresholds and safe-state response to optical faults.		

4.5 Optical luminescence and fluorescence quenching

Optical oxygen sensors use a luminophore whose emitted light is quenched by molecular oxygen. Intensity can be measured, but lifetime or phase methods are usually more robust because they are less dependent on absolute light intensity. The sensing chemistry is not consumed in the same way as electrochemical cells, although optical surfaces and coatings still need protection.

Strengths	Limitations	Best fit
Non-consumable principle, good long-term stability, fast response, strong diagnostic potential.	Requires pressure and temperature compensation; optical surface or coating contamination can bias readings.	Hydrogen, inerting, high-pressure gases, hazardous areas and duties where lower maintenance and fast response are valuable.

Optical luminescence oxygen measurement relies on quenching of a luminophore. Oxygen reduces the luminescence intensity and/or lifetime. Lifetime/phase techniques reduce sensitivity to optical intensity drift.

Degradation mechanisms are typically linked to optical surfaces, coating integrity, and compensation model validity rather than chemical consumption. This can reduce routine maintenance in applications where electrochemical sensors degrade quickly.

Critical design elements include temperature and pressure compensation, contamination control, and stable optical coupling. Because signal quality can be monitored, intrinsic diagnostics can be strong.

In safety integrity contexts, the analyzer must be specified with clear behavior upon diagnostic failure and with proof tests that validate both measurement and diagnostic action.

Optical Luminescence Oxygen Sensor

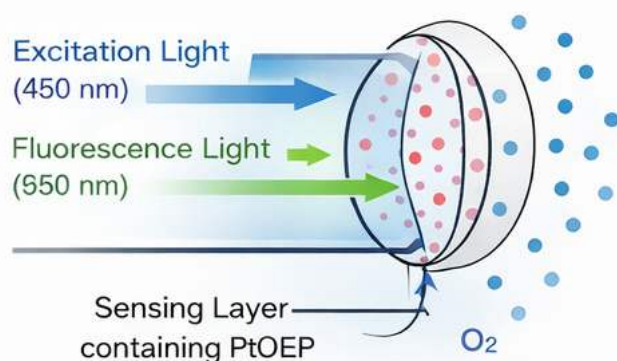


Fig. 7 – Optical luminescence oxygen sensor – quenching / lifetime detection

4.5.1 Safety integrity and SIL considerations

Lifetime-based approaches can offer strong diagnostic coverage (signal quality, lifetime plausibility, sensor temperature checks). Define safe-state behavior for out-of-range optical metrics and use proof tests to confirm that diagnostics trigger the defined safety response.

4.5.2 Failure-mode-focused SWOT (with diagnostic coverage)

Dimension	Key points	Typical fail-high behavior	Typical fail-low behavior
Strengths	Non-consumable principle; strong stability with lifetime methods; reduced flow dependence; strong diagnostics potential.		
Weaknesses	Requires T/P compensation; optical surfaces must remain clean; coating aging can change sensitivity.	Temperature miscompensation; phase measurement bias; optical reflections changing response.	Severe fouling; coating degradation; moisture films attenuating emission.
Opportunities	High-integrity hydrogen and inerting; long unattended operation; reduced sample-system complexity.		
Threats	Fouling/coating damage; miscompensation outside modeled envelope; poor installation thermal gradients.	Temperature miscompensation; phase measurement bias; optical reflections changing response.	Severe fouling; coating degradation; moisture films attenuating emission.
Diagnostics / Proof testing	High potential: lifetime plausibility, modulation depth, SNR. Proof tests should validate diagnostic thresholds and representative gas checks.		

4.6 GC, MS and indirect methods

Gas chromatography measures oxygen as one component of a separated multi-gas analysis. It is strong for quality assurance and composition reporting, but cycle times are usually too slow for fast protective functions. Mass spectrometry gives rapid multi-gas insight but needs vacuum/inlet integrity and careful calibration. Thermal conductivity can infer oxygen only where the matrix is stable and binary-like; it should not be treated as a selective oxygen method in variable mixtures.

Method	Main value	Main caution
Gas chromatography	Multi-component specification and audit trail.	Transport and cycle time make it unsuitable for fast trips.
Mass spectrometry	Rapid multi-gas diagnostics and optimisation.	Vacuum/inlet integrity, matrix effects and calibration complexity.
Thermal conductivity	Simple binary or near-binary measurement.	Non-selective; composition changes can masquerade as oxygen changes.
Wet chemistry / laboratory reference	Independent validation and dispute resolution.	Not continuous; sampling and preservation may dominate uncertainty.

GC measures oxygen as a component of a multi-gas analysis. Sample injection and separation enable selective quantification, but cycle time is typically minutes. GC is best for specification, auditing, and multi-component quality control rather than fast safety trips.

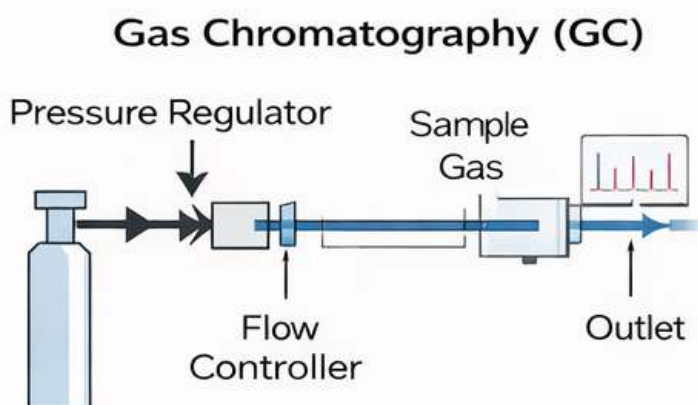


Fig. 8 – Gas chromatography overview – separation + detector

MS provides rapid multi-gas capability by measuring a mass spectrum. It is powerful for diagnostics and optimization, but requires vacuum/inlet integrity and robust calibration.

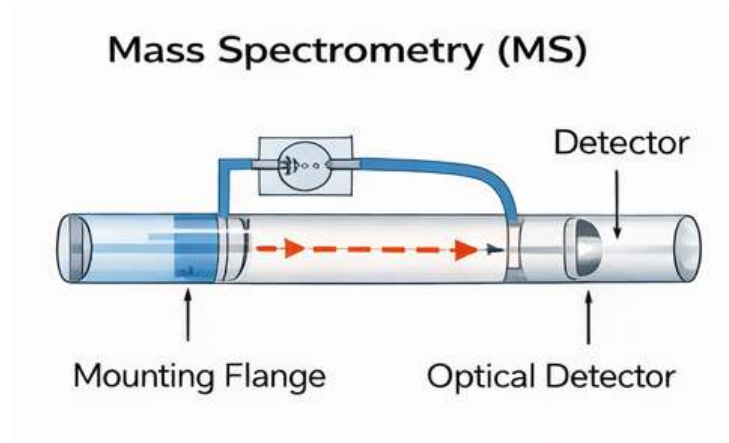


Fig. 9 – Mass spectrometry overview – ionization + m/z detection

TCD infers oxygen via bulk thermal conductivity changes and is not inherently selective. It is most appropriate for stable, binary-like mixtures and is generally not recommended for safety functions in variable matrices.

Thermal Conductivity Detector

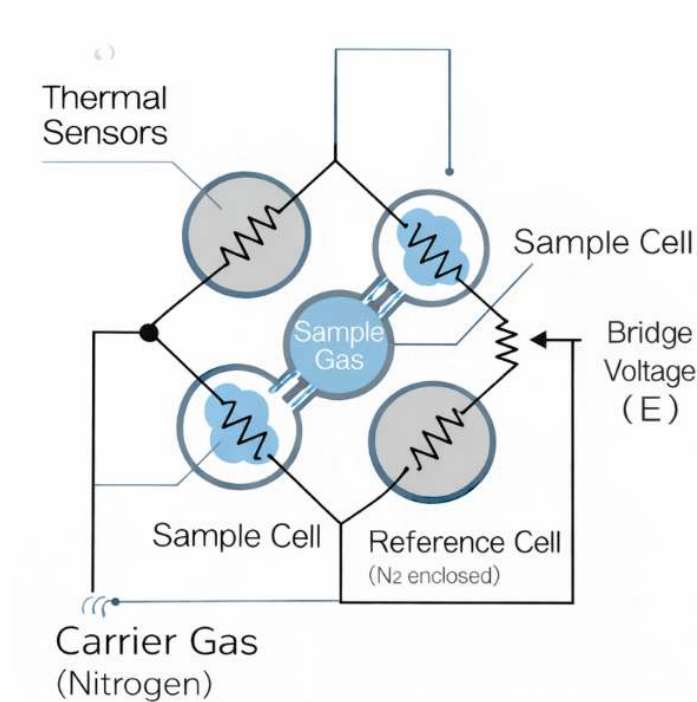


Fig. 10 – Thermal conductivity (TCD) – indirect measurement concept

5. Dissolved oxygen measurement

Dissolved oxygen has its own engineering rules. The measurement depends not only on oxygen concentration but also on solubility, temperature, salinity, pressure, fluid velocity and the boundary layer at the sensor surface.

Technology	Principle	Engineering notes
Clark-type electrochemical DO	Oxygen diffuses through a membrane and is reduced at a cathode.	Consumes oxygen; can depend on flow and membrane condition; regular electrolyte/membrane maintenance may be required.
Optical DO optode	Luminescence quenching at an oxygen-sensitive film.	Does not consume oxygen; less flow dependence; still requires temperature compensation and surface cleanliness.

Specification note: For process liquids, specify whether the instrument must report dissolved oxygen concentration, oxygen saturation or an equivalent gas-phase partial pressure. These choices are not administrative; they change the calibration and compensation model.

Clark-type DO sensors are amperometric devices where dissolved oxygen diffuses through a membrane and is reduced at a cathode. They consume oxygen, so measurement can depend on flow and boundary layer thickness.

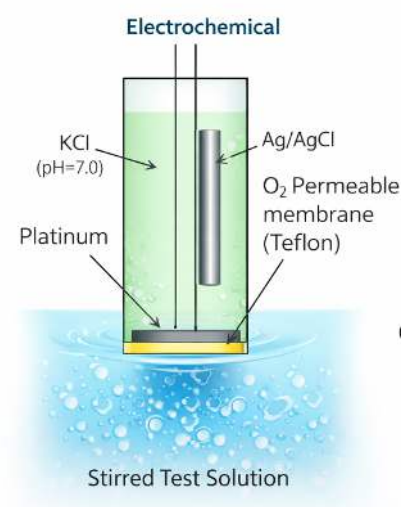


Fig. 12 – Clark-type DO sensor – membrane + electrochemistry

Optical DO uses luminescence quenching on an optode. Because oxygen is not consumed, optical DO reduces flow dependence and can provide improved stability for long deployments. Lifetime/phase methods improve robustness.

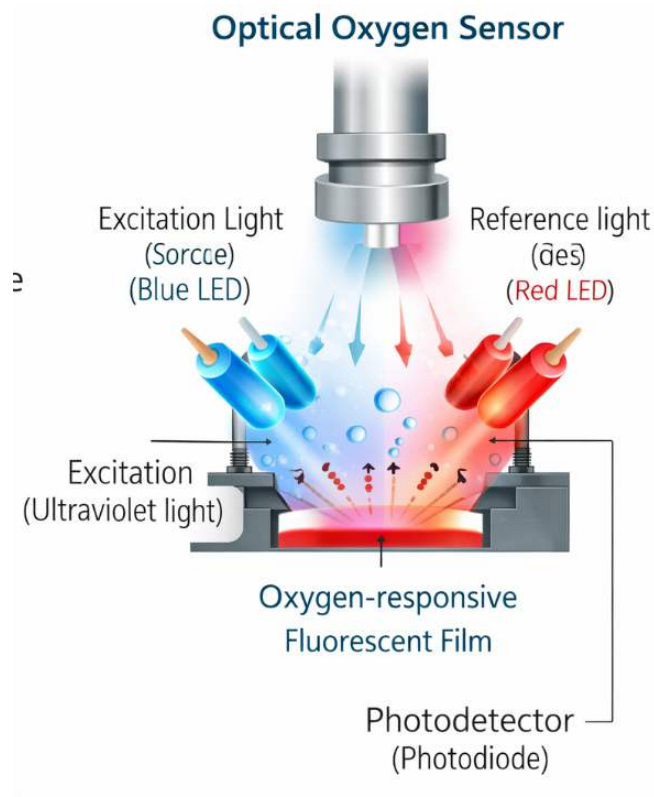
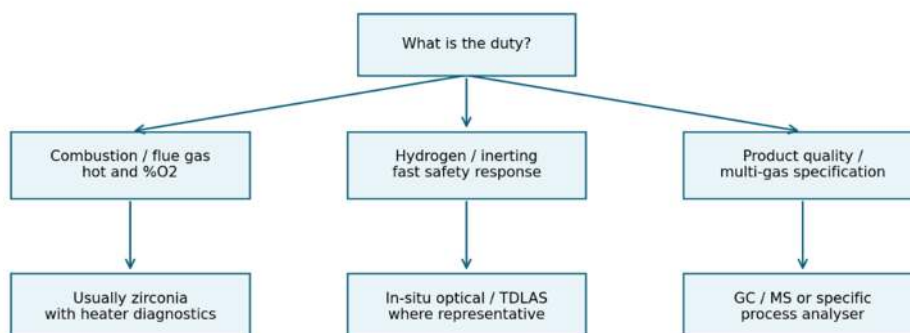


Fig. 13 – Optical DO sensor – optode + reader

6. Selection matrices and decision logic



Then check matrix effects, pressure, hazardous area, failure direction, proof-test access and lifecycle support.

6.1 Comparative Decision Tables

Duty	Most likely technology candidates	Key checks before selection
Trace O ₂ in high-pressure hydrogen	Optical luminescence, selected TDLAS, specialist high-pressure in-situ analyzer.	Pressure rating, hydrogen compatibility, hazardous area approval, response time, pressure compensation, proof-test method.
O ₂ in natural gas or sour gas	Optical luminescence, electrochemical in clean low-pressure systems, GC for composition.	H ₂ S compatibility, water dew point, condensate, pressure, corrosion materials, pipeline installation.
Combustion / flue gas	Zirconia, paramagnetic, TDLAS.	Temperature, particulates, reducing gases, soot, response, emissions reporting requirements.
Inerting of tanks or vessels	Paramagnetic, electrochemical, optical luminescence, TDLAS depending on cleanliness and speed.	Measurement location, response time, sample transport, LFL/LOC basis, fail-low hazard.
Multi-component product quality	GC, MS, process FTIR/NIR or specific analyzer package.	Cycle time, calibration gases, component list, sample integrity, custody requirements.
Dissolved oxygen in water	Clark-type DO or optical DO.	Flow dependence, fouling, temperature, salinity, cleaning, biological activity.

6.2 Comparative technology table

Technology	Typical range	Response	Diagnostics	Main risk
Electrochemical	ppm to %	Seconds to minutes including sampling	Limited intrinsic; proof testing essential	Consumable ageing and poisoning
Zirconia	% O ₂ , sometimes ppm in specialist designs	Fast in hot gas	Moderate; heater and impedance checks	Misuse outside combustion/hot gas envelope
Paramagnetic	% O ₂	Fast in clean sample	Moderate; relies on sample conditioning alarms	Wet or dirty sample bias
TDLAS	ppm to %, path dependent	Very fast	High optical diagnostics	Window fouling and alignment
Optical luminescence	ppm to 100% depending on design	Fast	High potential via lifetime, signal and temperature checks	Optical surface contamination or model limits
GC	ppm to % component reporting	Minutes	Chromatographic QA metrics	Not suitable for fast safety trips
MS	ppm to % multi-gas	Seconds	Internal checks plus calibration	Vacuum/inlet and matrix effects
TCD	Matrix dependent	Fast	Low as oxygen-specific measurement	Non-selective composition sensitivity

When comparing technologies, it's useful to answer these questions:

- What decision will be made based on this oxygen measurement?
- What happens if the analyzer reports a false high or a false low value?
- What is the required detection time for the application?

- Which process conditions (pressure, temperature, contaminants, humidity) are expected during both normal and peak operation?
- Can the process be measured directly, or cannot an extractive sample system be avoided?
- Which maintenance philosophy is acceptable for your process (e.g. routine sensing element replacement, periodic calibration or minimal intervention)?
- Are hazardous-area approvals and SIL coverage required?

7. Safety integrity, failure modes and proof testing

When oxygen measurement is used in a safety instrumented function, the measurement must be specified as part of the complete SIF. The question is not whether an analyzer has an attractive certificate. The question is whether the installed loop can detect the hazardous condition within the process safety time and go to the defined safe state with the required probability of dangerous failure.

Safety term	Engineering meaning for oxygen measurement
SIF	A specific safety instrumented function, for example trip hydrogen production on high oxygen in the hydrogen product stream.
SIL	A target risk reduction level for the SIF, not a marketing label for a standalone instrument.
Dangerous failure	A failure that prevents the SIF from acting when required. In inerting, a false low oxygen reading may be dangerous.
Safe failure	A failure that drives the system to a safe state or is detected and handled by the safety logic.
Diagnostic coverage	The fraction of relevant dangerous failures detected by internal or external diagnostics.
Proof test interval	The period between tests that reveal dangerous undetected failures; it must be justified, not guessed.

7.1 Fail-high and fail-low are application-specific

Application	Potential dangerous direction	Reason
Inerting of a vessel	Fail-low	The system may miss oxygen ingress and allow a flammable atmosphere.
Oxygen enrichment control	Fail-high or fail-low depending on duty	False high may shut a process; false low may permit unsafe enrichment.
Hydrogen product purity	Fail-low	Oxygen ingress/crossover may not be detected in time.
Combustion trim	Either direction can be harmful	False low can over-air or alter fuel/air control; false high can under-air and create CO/unburned fuel risk.
Confined space entry monitor	Both	False normal readings can expose personnel to oxygen deficiency, oxygen enrichment or flammable gas.

7.2 Proof testing guidance

2. Define the hazardous condition, trip point, allowed delay and safe state in the safety requirement specification.
3. Test the full loop where practical: sensor, transmitter, diagnostics, logic solver input, trip action and alarm handling.
4. Use challenge gases or validated simulation methods that prove the dangerous direction of failure can be detected.
5. Record as-found values before adjustment. An as-found drift trend is often more valuable than the corrected number.
6. Confirm diagnostic faults drive the required alarm or safe state, not only a local message on the analyzer.
7. Review bypass management, maintenance overrides and proof-test deferrals. They are small paperwork items until they are not.

Safety lifecycle note: Safety standards such as IEC 61508 and IEC 61511 require lifecycle thinking. For oxygen analyzers this means the sample system or in-situ installation, diagnostic wiring and proof-test access should be inside the engineering boundary, not treated as accessories.

8. Commissioning, calibration and maintenance

8.1 Commissioning checklist

Check	Acceptance evidence
Measurement basis	Range, units, dry/wet basis, pressure basis and compensation method are documented.
Process conditions	Normal, minimum, maximum and upset pressure/temperature/composition are known.
Location	Tap or insertion point is representative and accessible.
Leak integrity	Leak test sensitivity is appropriate for the required oxygen range.
Purge practice	Purge time clears dead volume and adsorbed oxygen; procedure is written.
Calibration gases	Certificates are traceable; uncertainty and balance gas are acceptable.
Firmware and configuration	Firmware version, analyzer configuration, communication parameters, compensation settings have been verified against the approved product documentation.
Diagnostics	Alarms are mapped to DCS/SIS and tested.
As-found/as-left	Records are captured before and after adjustment.
Bypass control	SIS bypass or maintenance override procedure is approved.
Training	Operators know which faults are process alarms and which are instrument health alarms.

8.2 Calibration strategy

Calibration should not be a ritual. It should test the measurement at the points that matter for operation and safety. A two-point calibration may be sufficient for some instruments, while others need factory characterisation plus field validation at one or more application-relevant points.

Calibration item	Engineering detail
Zero gas	Use oxygen-free or sufficiently low oxygen gas. Confirm the zero gas specification is below the required detection limit.
Span gas	Choose concentration near the operating point or trip point where possible.
Balance gas	Match process matrix where cross-sensitivity or quenching behaviour depends on gas composition.
Pressure	Validate at operating pressure where the technology is pressure-sensitive.
Temperature	Allow thermal stabilisation and verify compensation inputs.
Documentation	Record cylinder ID, certificate uncertainty, regulator and tubing configuration, flow, pressure and ambient conditions.

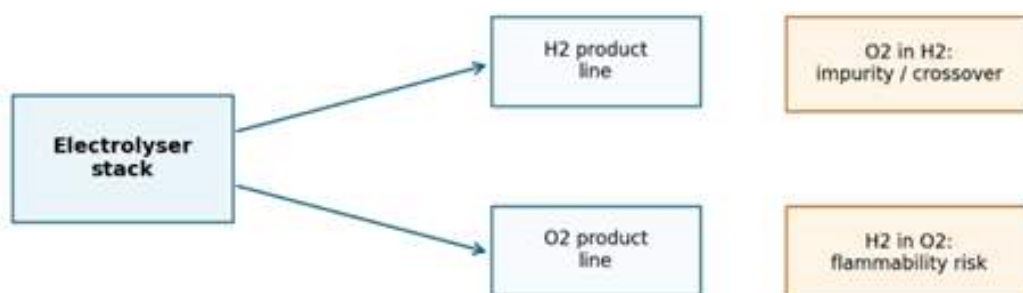


Fig. 14 – Commissioning Checklist

9. Industrial applications

9.1 Hydrogen production, compression and storage

Hydrogen systems create a demanding oxygen measurement problem because oxygen can be both a product-quality impurity and a safety indicator. In electrolyzers, membrane or separator faults and pressure imbalance can allow gas crossover. In compression and storage, oxygen ingress can affect purity, corrosion, materials and safety margins.



Fast oxygen measurement increases available process safety time and supports stack protection, product purity and trip logic.

Measurement point	Why oxygen matters	Preferred measurement attributes
Hydrogen product outlet	Purity, crossover detection and downstream fuel-cell or process requirements.	Low ppm sensitivity, fast response, pressure compensation, hydrogen compatibility.
Oxygen product outlet	Hydrogen crossover into oxygen side is a flammability concern.	Fast response and reliable alarms; often complemented by hydrogen-in-oxygen measurement.
Compressor discharge	High pressure increases mechanical and leak-path demands.	Direct pressure capability or carefully engineered pressure let-down.
Storage and transfer	Air ingress and purge effectiveness.	Trace sensitivity, low dead volume, clear purge validation.

9.2 Natural gas, LNG, biogas and RNG

Oxygen in natural gas and biogas can indicate air ingress, poor upgrading performance or pipeline contamination. It may also contribute to corrosion, sulphur chemistry and contractual quality issues. The matrix can include methane, CO₂, H₂S, water vapour, siloxanes and heavier hydrocarbons; technology selection must be made on the real stream, not a tidy brochure gas.

Service	Oxygen measurement reason	Special concerns
Natural gas transmission	Pipeline quality, corrosion management, air ingress detection.	Pressure, water dew point, H ₂ S, hydrocarbon condensate.
LNG facilities	Purge and inerting, process safety, product quality.	Cryogenic interfaces normally need extractive conditioning and careful sample design.
Biogas upgrading	Air ingress, biological process control, biomethane quality.	Moisture, H ₂ S, CO ₂ , siloxanes and fouling.
RNG injection	Network specification and safety.	Trace oxygen and response time at variable flow.

9.3 Refineries and petrochemical plants

Refinery and petrochemical oxygen measurements cover fired equipment, nitrogen blanketing, catalyst protection, flare and purge systems, process vents and product quality. The same site may need zirconia in a furnace, paramagnetic oxygen in clean inert gas, optical oxygen in high-pressure gas and GC for multi-component product verification.

9.4 Industrial gases and air separation

Air separation and industrial gas plants rely on oxygen measurement for purity control, enrichment, nitrogen product quality, argon processing and safety interlocks. Paramagnetic technology is common in clean percent-level streams, while trace oxygen duties often use electrochemical or optical methods depending on pressure, cleanliness and maintenance philosophy.

9.5 Combustion, emissions and fired heaters

Oxygen trim in combustion balances efficiency, emissions and safety. Too much excess air wastes energy and can reduce efficiency; too little air can create carbon monoxide, unburned fuel and unstable combustion. Zirconia and TDLAS are common candidates, but installation temperature, particulates, corrosive flue gas and maintenance access decide the final engineering answer.



10 Advanced Photonics-Based Measurement Principle

Advanced photonics technology utilizing luminescence quenching of a specially designed sensor dye. The sensing dye is immobilized on a robust support foil, forming a stable and highly selective sensing layer.

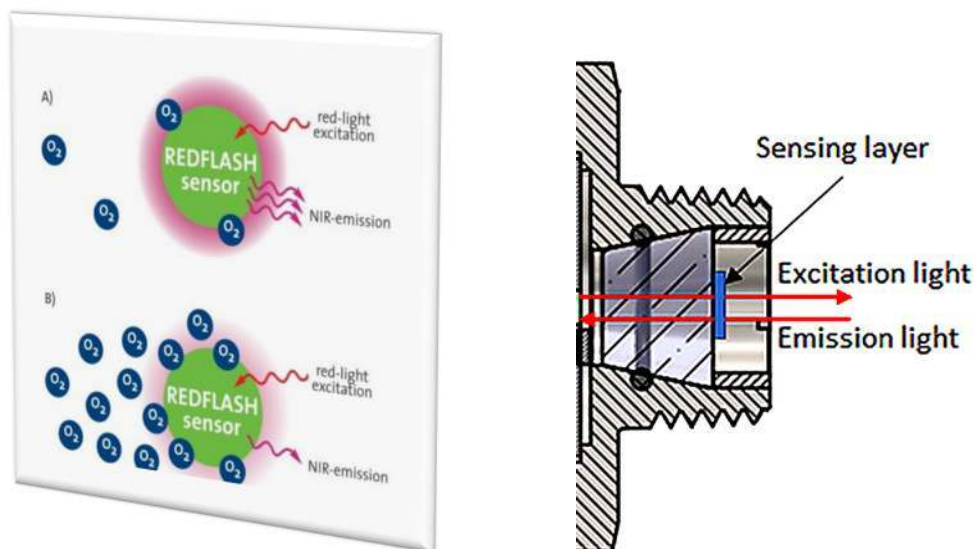


Fig. 15 – Luminescence quenching principle

This optical principle is inherently stable, drift-free, and immune to many of the limitations associated with electrochemical, paramagnetic, zirconia or TDL-based oxygen analyzers—especially under high pressure.

- The sensing layer is stimulated with red light emitted from an integrated optical source.
- The dye responds by emitting luminescence in the near-infrared (NIR) region of the electromagnetic spectrum.
- When molecular oxygen is present, it interacts with the excited dye molecules and quenches the luminescence.
- This quenching causes a reversible change in both luminescence intensity and lifetime, which is directly proportional to the oxygen concentration.
- The MOD-1040 precisely analyzes these optical changes to determine the true oxygen content in real time.

10.1 MOD-1040 optical oxygen analyzer technical profile

The MOD-1040 is included here as a specific example of an in-situ optical oxygen analyzer for high-pressure industrial gases. The description is application-oriented: the underlying

project decision should still be based on stream composition, pressure, temperature, hazardous area classification, safety function, response time and maintainability.

Parameter	Typical capability / engineering relevance
Measurement range	1 ppm to 100% O ₂ on a single platform.
Response	T90 below 5 seconds where the installation is representative.
Installation concept	Direct in-situ measurement without extractive sample conditioning.
Pressure capability	Up to 350 barg process pressure. Built-in automatic pressure calibration.
Hazardous area	ATEX / IECEx Zone 1 certified; SIL 2 certified according to product information.
Integration	4-20 mA, Modbus and Bluetooth commissioning/diagnostics options.
Materials	Stainless steel and selected corrosion-resistant wetted material options for demanding gases.
Typical applications	Hydrogen, electrolyser systems, natural gas, biogas/RNG, refineries, petrochemicals and industrial gases.

10.2 Where direct high-pressure measurement changes the design

No pressure reduction station is required solely for oxygen measurement, reducing hydrogen venting and sample handling.

- Transport delay is avoided, which can increase available process safety time.
- Leak paths from sample tubing, filters, pumps and analyzer houses are reduced.
- The mechanical nozzle, isolation method and maintenance access become central design items.
- The proof-test method must be planned at design stage because the analyzer is installed directly on the process.

The MOD-1040 Process Oxygen Analyzer is a high-performance, in-situ measurement solution engineered for accurate and reliable oxygen analysis directly in high-pressure gas pipelines. Designed for safety-critical and mission-critical applications, the MOD-1040 eliminates the need for gas sample extraction, conditioning systems, or pressure reduction—fundamentally changing how oxygen is measured in hazardous and high-integrity process environments.

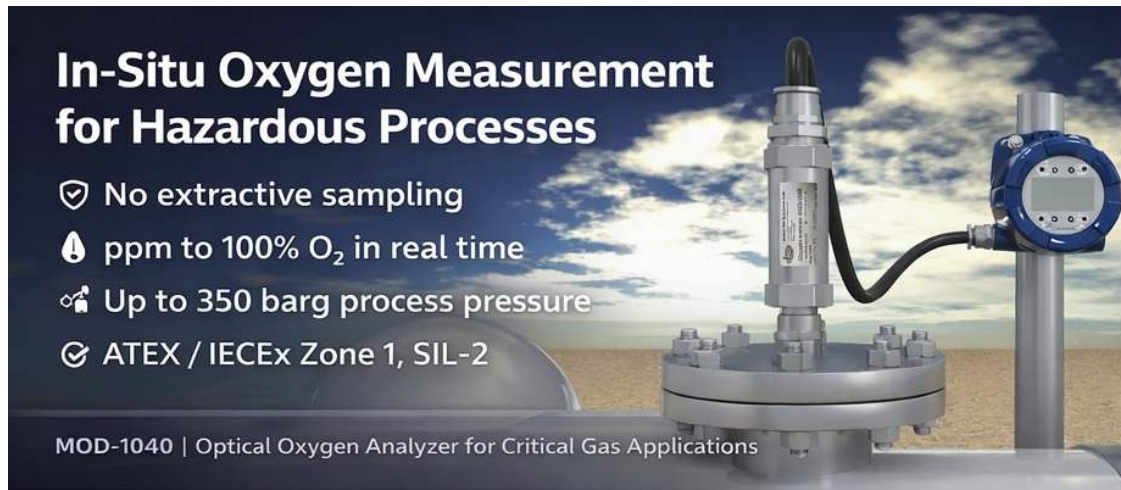


Fig. 16 – MOD-1040 Optical Oxygen Analyzer

By combining advanced photonics-based sensing with rugged, explosion-proof construction, the MOD-1040 delivers precise oxygen measurements across the full concentration range—from trace ppm levels to 100% O₂—even under extreme pressure, temperature, and environmental conditions. This makes the MOD-1040 particularly well suited for hydrogen production, hydrogen compression and storage, natural gas and refinery processes, chemical production units, and industrial gas systems, where oxygen ingress represents a critical safety, quality and reliability risk.

10.3 Field-Replaceable Optical Sensor Architecture

The sensor technology is implemented as a compact, plug-in optical module, specifically designed for industrial field conditions:

- No electrolyte consumption
- No membrane degradation
- Easily replaceable sensor spot
- No frequent recalibration cycles

An integrated infrared light source excites the sensing layer, while the emitted near-infrared luminescence is detected and analyzed internally. The fully reversible quenching mechanism ensures long-term stability and consistent performance across a wide range of operating conditions.

10.4 True In-Situ Oxygen Measurement—Without Sample Extraction

Industrial gas and hydrogen production systems often operate in high-pressure, hazardous zones, where minimizing leak paths is a primary safety objective. Traditional oxygen analysis technologies are not designed to withstand such conditions and therefore rely on sample extraction, pressure reduction, and conditioning systems—introducing additional failure points, maintenance burden, and safety risks.

The MOD-1040 overcomes these limitations by enabling direct, in-situ oxygen measurement inside the process pipeline, even at very high pressures. This capability:

- Eliminates sample systems entirely
- Reduces potential leak points
- Simplifies hazardous area classification
- Lowers installation and lifecycle costs
- Improves measurement response time and reliability

As a result, MOD-1040 allows engineers to confidently deploy oxygen measurement even in locations previously considered impractical or unsafe.

10.5 Engineered for Hydrogen and Safety-Critical Applications

In green and blue hydrogen production, oxygen contamination can lead to:

- Increased explosion risk
- Catalyst degradation
- Reduced product purity
- Accelerated material aging

The MOD-1040 is specifically engineered to address these challenges. Its optical sensing technology is ideally suited for hydrogen service, offering fast response, high selectivity, and intrinsic safety, even under pressures reaching hundreds of bar.

Automatic pressure and temperature compensation ensures that the reported oxygen concentration reflects true process conditions, not measurement artifacts caused by fluctuating operating parameters.



10.6 Key Capabilities and Technical Specifications

Measurement Performance:

- In-situ oxygen measurement range: 1 ppm to 100% O₂
- Response time (T90): < 5 seconds
- Automatic pressure and temperature compensation

Operating Conditions:

- Maximum operating pressure: up to 350 barg
- Ambient temperature range: –10 to +60 °C
- Designed for continuous operation in harsh industrial environments

Safety and Compliance:

- Explosion-proof certification: II 2 G Ex db IIC T4 Gb
- SIL-2 certified in accordance with IEC 61508-2:2010
- Suitable for ATEX / IECEx Zone 1 installations

Integration and Connectivity:

- Modbus communication for DCS, PLC and HMI systems
- Bluetooth interface for commissioning, diagnostics and maintenance
- Industrial-standard 4–20 mA analog inputs and outputs, enabling seamless integration with pressure and temperature transmitters and direct communication with DCS, PLC and safety shutdown systems.
- Compact, rugged design for direct pipe mounting

10.7 A New Standard for Oxygen Analysis in High-Pressure Processes

The MOD-1040 Process Oxygen Analyzer is not simply another analyzer option—it represents a step change in how oxygen is measured in high-pressure and hazardous environments. By combining photonics-based luminescence quenching, in-situ installation, and uncompromising safety certifications, the MOD-1040 enables safer plant designs, higher measurement integrity, and lower total cost of ownership.

For hydrogen production, refinery operations, and advanced industrial gas systems, the MOD-1040 sets a new benchmark for precision, safety, and operational efficiency

10.8 Calibration, Validation and Installation

Accurate oxygen measurement in industrial processes is not solely a function of sensor technology; it is equally governed by calibration philosophy, installation quality, and ongoing validation practices. In safety-critical and asset-integrity-driven applications, oxygen analyzers must be treated as metrological instruments embedded within a broader process system, rather than as standalone devices.



11 Calibration Strategy and Traceability

For in-situ oxygen analyzers, calibration philosophy differs fundamentally from extractive systems. Because the measurement is performed directly at process conditions—pressure, temperature, and composition—calibration gases do not need to replicate the full process matrix, but must be traceable, stable, and applied in a controlled manner.

Best practice includes:

- Zero verification using oxygen-free or oxygen-depleted gases (e.g., nitrogen or hydrogen-rich purge streams).
- Span verification using certified oxygen mixtures selected to bracket the relevant operating range rather than full-scale values.
- Documentation of as-found and as-left values, enabling trend-based assessment of sensor drift rather than periodic recalibration alone.

Optical oxygen measurement technologies, in particular, benefit from calibration approaches that decouple sensor physics from gas transport effects, allowing longer calibration intervals and reducing dependency on frequent manual intervention.

11.1 Validation and Functional Testing

Validation extends beyond calibration accuracy and must address whether the analyzer continues to perform its intended function under real operating conditions. This is especially critical in trace-oxygen and safety-related applications.

Recommended validation practices include:

- Verification of response time under representative process dynamics.
- Monitoring of internal diagnostics such as optical signal strength, excitation source health, and temperature stability.
- Periodic challenge tests aligned with the defined proof-test interval for safety instrumented functions (SIFs), where applicable.

Validation should confirm not only measurement correctness but also fault detectability, ensuring that internal failures are identified before they compromise process safety or asset integrity.

11.2 Installation and Process Interface Design

Installation quality often dominates real-world performance, particularly for trace oxygen applications. In-situ analyzers eliminate transport delay and many leak paths associated with extractive systems, but they require careful attention to the process interface.

Key installation considerations include:

- Selection of locations with representative flow and composition, avoiding stagnant zones and boundary layers.
- Mechanical design that prevents air ingress during maintenance, pressure cycling, or thermal contraction.



- Control of surface finishes and materials to minimize oxygen adsorption and desorption, which can distort low-ppm measurements.

When properly installed, in-situ analyzers provide a more faithful representation of process oxygen activity than downstream sampling systems, particularly in high-pressure and hydrogen-rich environments.

11.3 Balance-of-Plant (BoP) Perspective: Oxygen, Hydrogen, and Intelligence

Modern hydrogen and energy systems increasingly rely on integrated Balance-of-Plant architectures, where multiple analyzers and sensors feed higher-level optimization and safety logic. Within this context, oxygen measurement plays a pivotal role.

A coordinated BoP approach typically integrates:

- Oxygen analysis for inerting, safety, and corrosion control.
- Hydrogen analysis for purity, leak detection, and process efficiency.
- Advanced analytics or AI-based models that correlate sensor data with operational outcomes.

In such architectures, oxygen is often the leading safety variable—its presence defines ignition risk, material compatibility, and allowable operating envelopes. High-integrity, in-situ oxygen measurement therefore becomes a cornerstone of system-level intelligence, enabling faster response, reduced uncertainty, and more resilient operation.

12. Applications of Oxygen Measurement in Industrial Processes

Oxygen measurement is a foundational safety, quality, and reliability function across a wide range of process industries. While the physical measurement principle may be similar, the role oxygen plays, the acceptable limits, and the consequences of failure vary significantly by application. This chapter reviews key industrial use cases, emphasizing how process conditions, safety objectives, and system design requirements shape oxygen analyzer selection and deployment.

12.1 Natural Gas Processing and Transmission

Role of Oxygen Measurement

In natural gas production, processing, and transmission systems, oxygen is considered a contaminant. Even trace concentrations can introduce multiple risks:

- Corrosion acceleration, particularly in the presence of moisture and acid gases (CO_2 , H_2S)
- Degradation of pipeline materials and compressor components
- Increased explosion risk during maintenance, purging, or upset conditions
- Catalyst poisoning in downstream processing units

Oxygen may enter natural gas systems through:

- Air ingress during maintenance or pigging
- Leaks in compressor seals or sampling systems
- Inadequate purging during startup or shutdown
- Interface with atmospheric storage or blending operations

Measurement Challenges

Natural gas environments are technically demanding:

- High pressures (often >100 barg)
- Variable composition (methane, ethane, heavier hydrocarbons)
- Presence of CO_2 , H_2S , and water vapor
- Risk of adsorption/desorption effects at trace oxygen levels

In such systems, sample system integrity often dominates overall measurement uncertainty, particularly when oxygen limits are in the low ppmv range.

Implementation Considerations

- Oxygen is typically monitored continuously at critical points such as compressor discharge, dehydration outlets, or custody-transfer interfaces.
- Measurement ranges often span from ppmv to low % v/v, depending on system function.
- Analyzer installations must comply with hazardous-area requirements (Zone 1 / Class I Div 1).
- Diagnostics are essential to distinguish true oxygen ingress from analyzer or sampling faults.



Optical in-situ or high-integrity extractive analyzers (e.g., MOD-1040 used as an example of this class) are often selected because they minimize sample handling and reduce air ingress risk.

12.2 Hydrogen Production, Processing, and Storage

Safety Context

Hydrogen presents one of the most demanding safety environments for oxygen measurement. Its:

- Extremely low ignition energy
- Wide flammability range
- High diffusivity

mean that even small oxygen concentrations can create hazardous mixtures.

Hydrogen is produced through multiple pathways:

- Steam Methane Reforming (SMR)
- Water electrolysis (alkaline, PEM, SOEC)
- Biomass gasification
- Reforming of renewable feedstocks

Across all routes, oxygen control is essential to maintain concentrations well below the Limiting Oxygen Concentration (LOC).

Measurement Objectives

Oxygen monitoring in hydrogen systems serves to:

- Prevent formation of flammable or detonable mixtures
- Verify inerting effectiveness
- Detect air ingress in high-pressure systems
- Support safe startup, shutdown, and maintenance procedures

Applications include:

- Hydrogen dryers and purifiers
- High-pressure hydrogen compressors
- Storage vessels and tube trailers
- Distribution pipelines
- Fuel cell supply systems

Technical Challenges

- Pressures commonly exceed 200 barg
- Hydrogen's low molecular weight complicates extractive sampling
- Traditional electrochemical sensors may be unsuitable due to cross-sensitivity or lifetime limitations
- Fail-safe behavior is critical: fail-low can be dangerous if oxygen ingress goes undetected



System Design Implications

- Analyzer selection must consider failure direction, diagnostic coverage, and proof-test strategy.
- In many hydrogen safety functions, analyzers are part of a Safety Instrumented Function (SIF) rather than purely operational monitoring.
- Technologies that do not consume oxygen and that operate without pressure reduction are often preferred.

In this context, advanced optical analyzers (such as MOD-1040-type systems) are frequently deployed as part of integrated hydrogen safety architectures.

12.3 Chemical and Petrochemical Processing

Process Role of Oxygen

In chemical and petrochemical plants, oxygen measurement supports:

- Explosion prevention in reactors and storage vessels
- Inerting verification during batch operations
- Protection of flammable solvent systems
- Compliance with safety and environmental regulations

Oxygen limits are often defined by:

- Material safety data
- Process hazard analysis (PHA)
- Layer of Protection Analysis (LOPA)
- Insurance and regulatory requirements

Typical Applications

- Reactor headspace monitoring
- Nitrogen inerting systems
- Solvent storage tanks
- Polymerization units
- Distillation columns handling flammable feeds

Measurement Requirements

- Rapid response during transient events
- Reliable operation across wide temperature ranges
- Resistance to solvent vapors and process contaminants
- Integration with control and safety systems

In many chemical applications, oxygen analyzers are used in dual roles:

- As control inputs for inert gas flow
- As independent safeguards triggering alarms or trips

The ability to clearly diagnose sensor health and distinguish process upsets from analyzer faults is essential.



12.4 High-Pressure Gas Production and Processing

Importance of Pressure Capability

Many modern gas-processing applications operate at elevated pressures to:

- Improve energy efficiency
- Reduce equipment size
- Enable downstream compression or storage

However, pressure significantly influences:

- Oxygen partial pressure
- Gas density and diffusion behavior
- Mechanical stress on analyzer components

Design Implications

- Pressure reduction prior to measurement introduces:
 - Transport delay
 - Additional leak paths
 - Potential oxygen enrichment in trapped volumes
- High-pressure-capable analyzers allow:
 - Direct measurement at process pressure
 - Improved safety integrity
 - Faster response times

Systems designed for operation up to 200 barg and beyond (as exemplified by MOD-1040-class analyzers) address these challenges by eliminating pressure letdown and minimizing sample-system complexity.

12.5 Cross-Application Considerations

Regardless of industry, several principles apply universally:

- Oxygen analyzers must be evaluated as complete systems, not standalone sensors.
- Trace oxygen applications are often limited by:
 - Air ingress
 - Adsorption/desorption
 - Sample transport delay
- Safety relevance depends on:
 - Failure mode (fail-high vs fail-low)
 - Diagnostic capability
 - Integration with safety logic
- Technology selection should follow the Safety Requirement Specification (SRS), not vice versa.



13. Engineering specification template

The following template can be used as a starting point for enquiries, datasheets or internal project reviews. It is deliberately practical. Missing information here usually appears later as a commissioning problem.

Field	Required project information
Tag number and service	Process name, unit, duty, quality/control/safety classification.
Measured variable	Oxygen unit, range, alarm/trip points, required resolution and accuracy.
Stream composition	Normal and upset composition, including water, H ₂ S, CO ₂ , hydrocarbons, dust, aerosols and corrosives.
Process conditions	Inlet/outlet pressure and temperature normal/min/max; phase; velocity; condensation risk, corrosivity.
Installation	In-situ or extractive, tap/nozzle details, sample line length, analyzer shelter requirement.
Area classification	Zone/division, gas group, temperature class, ingress protection and ambient temperature.
Response requirement	Sensor response, total loop response and process safety time if applicable.
Outputs and integration	4-20 mA, Modbus, HART, relays, diagnostics, DCS/SIS mapping.
Calibration and proof test	Gases, method, frequency, access, bypass procedure and records.
Documentation	Certificates, manuals, hazardous area certificates, SIL data, FAT/SAT procedure, drawings.

14 FAT and SAT acceptance items

FAT and SAT should confirm that the oxygen analyzer, sampling arrangement and integration into the control or safety system fully match the approved specification. The



analyzer model, hardware configuration, tag number, measurement range, engineering units, output scaling, alarm settings, diagnostic functions and communication map shall be checked against the datasheet, I/O list, cause-and-effect chart and project documentation. Any deviation shall be recorded and formally accepted before release.

Calibration documentation shall be reviewed before testing. This includes factory calibration certificates, traceability of reference gases, gas cylinder composition, expiry date, stated uncertainty and compatibility with the required measuring range and accuracy. The uncertainty of the calibration gas should be sufficiently lower than the specified analyzer accuracy, otherwise the test result may look precise while proving very little.

Zero, span and application-specific response checks shall be performed using approved test gases or a defined process simulation method. The test record shall include as-found values, adjustment details where applicable, as-left values, response time, stability and any observed drift. For trace oxygen applications, special attention shall be given to purge time, dead volume, leakage and adsorption effects, as these often dominate the practical test result.

Where the analyzer is connected to alarms, shutdown logic or a safety function, diagnostic alarms and safe-state behaviour shall be demonstrated. This may include sensor fault, low signal, loss of power, communication failure, sample flow failure, pressure deviation, optical fault, calibration failure or other configured diagnostic conditions. The response shall be verified against the cause-and-effect chart and the safety requirement specification, including the correct alarm priority, output status and DCS, PLC or SIS indication.

Mechanical and electrical checks shall confirm materials of construction, wetted parts, pressure rating, process connection, gasket compatibility, hazardous-area marking, cable glands, earthing, enclosure protection, nameplate data and certification. The installed equipment shall be checked against the hazardous-area classification and project installation standard.

For extractive oxygen analyzer systems, the sample system shall be tested as part of the measurement loop, not treated as an accessory. Sample flow, pressure regulation, filtration, condensation control, leak integrity, purge arrangement, vent routing, bypass flow, drain connection and safe disposal of calibration gases shall be verified. The test shall also confirm that the sample reaching the analyzer is representative of the process and that sample transport delay is acceptable for the intended control or safety function.

For in-situ oxygen analyzer systems, the insertion assembly, isolation valve, sealing arrangement, probe orientation, insertion depth, mechanical support and maintenance clearance shall be checked. The installation shall allow safe removal, inspection and replacement of the sensing element where applicable. Process temperature, pressure, flow direction, vibration, condensation risk and access for calibration or validation shall be confirmed before SAT acceptance.

14. Glossary

Term	Definition
Adsorption/desorption	Attachment and release of oxygen on surfaces in tubing, regulators or sensor cavities; important at trace levels.
APC	Advanced process control; may use analyzer data to optimise process operation.
Dead volume	Internal volume that is poorly swept by sample flow and therefore slows response or retains previous gas.
Diagnostic coverage	Share of relevant dangerous failures detected by diagnostics.
Fail-high / fail-low	Failure direction in which indicated oxygen is higher or lower than the true value.
Hazardous area	Area where explosive gas atmosphere may be present, requiring certified equipment and installation practice.
In-situ	Measurement made directly in the process without extracting a continuous sample to a remote analyzer.
LOC	Limiting oxygen concentration below which combustion is not supported for a defined fuel/inert system.
SIF	Safety instrumented function: a specific protective action implemented by sensor, logic solver and final element.
SIL	Safety integrity level: target risk reduction level for a safety function.
Stern-Volmer relationship	Classical relationship used to describe quenching of luminescence by oxygen or other quenchers.
T90	Time to reach 90% of final value after a step change.

TDLAS	Tunable diode laser absorption spectroscopy.
Wet basis	Gas concentration reported including water vapour in the total gas composition.

15. References and further reading

Modcon Systems Ltd., MOD-1040 Oxygen Analyzer product page, accessed June 2026.
Provides product range, pressure, response, approvals and application information.

OSHA 29 CFR 1910.146, Permit-required confined spaces. Defines oxygen deficient and oxygen enriched atmospheres and requirements for atmospheric testing in confined spaces.

IEC 61508:2010, Functional safety of electrical/electronic/programmable electronic safety-related systems.

IEC 61511, Functional safety - safety instrumented systems for the process industry sector.

ISO 22734-1:2025, Hydrogen generators using water electrolysis - Part 1. Current standard replacing ISO 22734:2019.

ISO 14687:2025, Hydrogen fuel quality - Product specification. Current version replacing ISO 14687:2019.

Hydrogen Safety Best Practices / H2Tools and related hydrogen safety guidance on flammability, ventilation, leaks, purging and system design.

U. Michelucci, M. Baumgartner and F. Venturini, Optical oxygen sensing with artificial intelligence, 2020. Describes luminescence quenching and Stern-Volmer based oxygen sensing context.

General process analyzer engineering practice: sample conditioning, analyzer validation, proof testing, traceable calibration gases and lifecycle maintenance.

Source notes used in this revision

This revision is written as an engineering handbook rather than a datasheet. It combines the Rev.1.0 structure with expanded explanatory text, practical tables and current publicly available references. It does not replace project-specific HAZOP, LOPA, SRS, datasheet review, hazardous-area design or vendor-certified documentation.